**IS 12225: 2022**

*भारतीयमानक*

**सेन्ट्रीफ्यूगलजेटपंप—विशिष्टि**

( *दूसरापुनरीक्षण*)

*Indian Standard*

**CENTRIFUGAL JET PUMP — SPECIFICATION**

( *Second Revision* )

ICS 23.100.10

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**भारतीयमानकब्यूरो**

**B U R E A U OF I N D I A N S T A N D A R D S**

मानकभवन, 9 बहादुरशाहज़फरमार्ग, नईदिल्ली 110002

MANAK BHAVAN, 9 BAHADUR SHAH ZAFAR MARG,

NEW DELHI 110002

**November 2022Price Group**

Pumps Sectional Committee, MED20

FOREWORD

This Indian Standard (Second Revision) was adopted by the Bureau of Indian Standards, after the draft finalized by Pump Sectional Committee had been approved by the Mechanical Engineering Division Council.

As, for agricultural purposes, centrifugal jet pumps are generally used, the committee felt the need of preparing separate standard on centrifugal jet pumps.

This standard was first formulated in 1987 and subsequently revised in 1997.

This revision has been taken up to keep pace with the latest technological developments and practices followed in pump industry. This revision incorporates the following major changes, apart from incorporating the amendments issued to the last version of the standard:

1. A new clause**6** has been added and clause **10.3** has been modified;
2. Last line of clause **10.1** has been modified;

In the revision of this standard, considerable assistance has been obtained from the leading manufacturers and users in this country.

The composition of the committee responsible for the formulation of this standard is given in Annex E.

For the purpose of deciding whether a particular requirement of this standard is complied with, the final value, observed or calculated expressing the result of a test or analysis, shall be rounded off in accordance with IS 2: 2022 ‘Rules for rounding off numerical values (*second revision*).’ The number of significant places retained in the rounded-off value should be the same as that of the specified value in this standard.

*Indian Standard*

CENTRIFUGAL JET PUMP — SPECIFICATION

*(SecondRevision)*

1. **SCOPE**

This standard specifies the requirements of single and multistage centrifugal jet pump used for pumping water from wells beyond suction capacity of horizontal/vertical end suction centrifugal pumps.

**2REFERENCES**

The standards listed in Annex A, contain provisions which, through their reference in this text, constitute provisions of this standard. At the time of publication, the editions indicated were valid. All standards are subject to revision and parties to agreements based on this standard are encouraged to investigate the possibility of applying the most recent editions of the standards in Annex A.

**3 PRINCIPLE OF OPERATION OF CENTRIFUGAL JET PUMP**

Centrifugal jet pump is a combination of a centrifugal pump and a jet unit. This combination helps in lifting water from a depth beyond the suction lift capacity of the centrifugal pump alone.

The centrifugal pump (*see* Fig. 1) is primed, started and is made to operate on optimum total head. This head can be created by system delivery head or pressure regulating valve. For efficient operation of the combination, the maximum discharge head (delivery head of centrifugal pump) is to be maintained by adjusting the pressure regulating valve to a total head of centrifugal pump head minus six meters. A part of this pressurized water from the centrifugal jet pump passes through a pressure pipe to jet assembly nozzle. Above the nozzle, a venturi tube is fitted concentrically in the jet assembly body. The nozzle converts the pressure energy of the water into velocity energy.

This high velocity water from the nozzle enters the venture and accelerates the surrounding water in the annular area between nozzle and venturi, thereby creating vacuum in the annular area. Due to this vacuum, water is sucked from the well into the jet body through a foot valve. The momentum transfer takes place in the mixing throat of venturi. The kinetic energy of water is converted into pressure energy in the diverging portion of the venturi, called the diffuser. This pressurized water rises in the delivery pipe of the jet assembly, which in turn acts as a suction pipe of the centrifugal pump, to a level within the suction lift capacity of the centrifugal pump to enable the centrifugal pump to suck the water. The quantity drawn from well is delivered as net system discharge and the driving quantity is recirculated. The level from which the centrifugal pump sucks the water is taken as six metres below the centrifugal pump centre line as optimum level.



Fig. 1 Schematic Operational Diagram of aCentrifugal Jet Pump

****

|  |  |
| --- | --- |
| * 1. PrimingUnit
 | 6)Clamp  |
| * 1. PressureControlValve
 | 7)Jet Assembly |
| * 1. PressureGauge
 | 8)Foot Valve |
| * 1. MonosetPump
 | 9)Delivery Pipe Jet Pump (Suction Pipe of Centrifugal Pump) |
| * 1. SlipCoupling
 | 10)Pressure Pipe |

Fig. 2 Typical Installation for Twin Type Centrifugal Jet Pump

**4.2Duplex Type**

In duplex type of jet assembly, two concentric pipes are fitted to connect the centrifugal pump and jet assembly. The inner pipe acts as a delivery pipe of jet Assembly, which in turn is the suction pipe of centrifugal pump. The annular area between the outer pipe and the inner pipe acts as pressure pipe to supply water to the jet arrangement nozzle.

Similar to twin type jet assembly, delivery pipe (suction pipe of centrifugal pump) and outer pipe are screwed together to the jet assembly body and are lowered together. The concentric flow is bifurcated into a twin flow at the ground level by using a duplex head/well adopter, which is connected to the centrifugal pump (*see* Fig. 3).



|  |  |  |  |
| --- | --- | --- | --- |
| 1) | Priming Unit | 7) | Clamp |
| 2) | Pressure Control Valve | 8) | Jet Venturi |
| 3) | Pressure Gauge | 9) | Nozzle |
| 4) | Mono Pump | 10) | Foot Valve |
| 5) | Slip Coupling | 11) | Strainer |
| 6) | Duplex Head/Well Adopter |  |  |

Fig. 3 Typical Installation for Duplex Type Centrifugal Jet Pump

**4.3Packer Type**

The construction of the packer type arrangement is similar to the duplex type except that the bottom portion of the annular space between the two pipes below the nozzle is sealed through a packer housing (*see* Fig. 4 and Fig. 4A). The packers are bucket washer fitted to the bottom-most point of the jet unit. The packer housing is screwed at the bottom-most point of the outer pipe. This enables to lower outer pipe and then inner pipe independently thereby resulting in ease of installation.



|  |  |  |  |
| --- | --- | --- | --- |
| 1) | Primingunit | 7) | Clamp |
| 2) | Pressurecontrol valve | 8) | Jetpump venturi |
| 3) | Pressuregauge | 9) | Nozzle |
| 4) | Monopump | 10) | Footvalve |
| 5) | Slipcoupling | 11) | Deliverypipe jet pump/suction pipe of centrifugal pump |
| 6) | Packerhead | 12) | Pressurepipe |

Fig. 4 Typical Installation for Packer Type Centrifugal Jet Pump



Fig. 4aSection Through aPacker Type Jet Pump Assembly

**5PUMP AND PRIME MOVER FORCENTRIFUGAL JET PUMP**

**5.1Centrifugal Pumps**

Constructional features of the centrifugal pumps may conform to IS 6595 (Part 1) or IS 9079.

**5.2 Prime Movers**

**5.2.1** *Motor Drive*

In case of electric monoset pump, the motor shall conformto the testing requirements given in IS 9079 exceptfor temperature rise test. The temperature rise testshall be conducted at the maximum current, in theoperating Depth to Low Water Level (DLWL) range.The temperature rise shall not exceed the limits specified in Table 8 of IS 15999 (Part 1).

**5.2.2***Engine Drive*

In case of engine monoset the engine shallconform to IS 7347 or IS 10001 or IS 11170.

**5.2.3***Coupled and Belt Driven Set*

In case of coupled and belt driven sets calibrated primemover shall be used for the purpose of testing.

**6 OTHER GENERAL REQUIREMENTS**

**6.1** The pump shaft should be of adequate size to transmit the required power over the entire head range.

**6.2**If the pump casing is subjected to the hydrostatic test as per**10.3**, then during routine testing of the assembled pump, the packing and seal leakage detection may be done with pressurized air at 1 kg/cm2.

**6.3**Cables used shall be as per IS 694.

**6.4Voltage and Frequency Variation**

Motor of the monoset pumps shall be capable of delivering the rated output:

a) With the terminal voltage differing from its rated value by not more than +6 percent and -15 percent;

b) The frequency differing from its rated value by not more than ± 3 percent; and

c) Any combination of (a) and (b).

**7 MATERIAL OF CONSTRUCTION**

It is recognized that a number of materials of construction are available to meet the requirements for centrifugal jet pump. A few typical materials are indicated below for guidance of the manufacturer and the user.

| *Sl No.* | *Component* | *Materials of Construction* |
| --- | --- | --- |
| 1. 1)
 | Nozzle | Brass grade HTBI of IS 304 or bronze LTB2 of IS 318 or suitable thermoplastics such as polyphenylene oxide (PPO), polycarbonate (PC), acetal (polyacetals) resins, nylon 6 or nylon 66, glass filled nylon, stainless steel grade 04Cr13, 12Cr13, 20Cr13 of IS 6603, cast iron grade FG 200 of IS 210, polytetrafluoroethylene (PTFE), acrylonitrile butadiene styrene copolymers (ABS), polyethylene terephthalate (PET), ultra high molecular weight polyethylene (UHMWPE), etc. |
| 1. 2)
 | Venturi | Brass grade HTB1 of IS 304 or bronze LTB2 of IS 318 or suitable thermoplastics such as polyphenylene oxide (PPO), polycarbonate (PC), acetal (polyacetals) resins, nylon 6 or nylon 66, glass filled nylon,stainless steel grade 04Cr13, 12Cr13, 20Cr13 of IS 6603, cast iron grade FG 200 of IS 210, polytetrafluoroethylene (PTFE), acrylonitrilebutadiene styrene copolymers (ABS), polyethylene terephthalate (PET), ultra high molecular weight polyethylene (UHMWPE), etc. |
| 1. 3)
 | Foot valve | Bronze grade LTB2 of IS 318 or brass grade HTB1 of IS 304 or cast iron grade FG 200 of IS 210 or suitable thermoplastics such as polyphenylene oxide (PPO), polycarbonate (PC), acetal (polyacetals) resins, nylon 6 or nylon 66, glass filled nylon, polytetrafluoroethylene (PTFE), acrylonitrile butadiene styrene copolymers (ABS), polyethylene terephthalate (PET), ultra high molecular weight polyethylene (UHMWPE), etc. |
| 1. 4)
 | Strainer of foot valve | Brass grade HTB1 of IS 304 or suitable thermoplastics such as polypropylene, nylon 6 or nylon 66, cast iron grade FG 200 of IS 210, high density polyethylene (HDPE), low density polyethylene (LDPE), glass filled nylon, etc. |
| 1. 5)
 | Jet pump (assembly)body | Cast iron grade FG 200 of IS 210 or bronze grade LTB2 of IS 318 or brass grade HTB1 of IS 304 or suitable thermoplastics such as polyphenylene oxide (PPO), Polycarbonate (PC), acetal (polyacetals) resins, nylon 6 or nylon 66, glass filled nylon, polytetrafluoroethylene (PTFE), etc. |
| 1. 6)
 | Impeller | Brass grade HTB1 of IS 304 or bronze LTB2 of IS 318, cast iron grade FG 200 of IS 210 or suitable thermoplastics such as polyphenylene oxide (PPO), polycarbonate (PC), acetal(polyacetals) resins, nylon 6 or nylon 66, glass filled nylon, polytetrafluoroethylene (PTFE), acrylonitrile butadiene styrene copolymers (ABS), polyethylene terephthalate (PET), ultra high molecular weight polyethylene (UHMWPE), etc. |
| 1. 7)
 | Casing | Cast iron grade FG 200 of IS 210 or corrosive resistance alloy steel and nickel base casting for general application (*see* IS 3444) suitable plastic or aluminium magnesium alloys. |
| 1. 8)
 | Pressure regulating valvea) Body b) Diaphragmc) Valve seat | Brass grade HTB1 of IS 304 or bronze LTB2 of IS 318 or suitable thermoplastics such as polyphenylene oxide (PPO), polycarbonate, acetal (polyacetals) resins, nylon 6 or nylon 66, glass filled nylon,stainless steel grade 04Cr13, 12Cr13, 20Cr13 of IS 6603, cast iron grade FG 200 of IS 210, polytetrafluoroethylene (PTFE), acrylonitrile butadiene styrene copolymers (ABS), polyethylene terephthalate (PET), ultra high molecular weight polyethylene (UHMWPE), etc.Neoprene rubber or nitrile rubber.Bronze grade LTB2 of IS 318 or suitable thermoplastics such as polyphenylene oxide (PPO), polycarbonate (PC), acetal (polyacetals) resins, nylon 6 or nylon 66, glass filled nylon, polytetrafluoroethylene (PTFE), acrylonitrile butadiene styrene copolymer (ABS), polyethylene terephthalate (PET), ultra high molecular weight polyethylene (UHMWPE), etc. |
| 1. 9.
 | Slip coupling (optional) for twin typea) Body b) Sealing ring | Cast iron grade FG 200 of IS 210.Neoprene rubber or nitrile rubber. |
| 1. 10.
 | Packer head/duplex head and flanges | Cast iron grade FG 200 of IS 210. |

NOTES

## **1** The materials listed are to be considered as only typical and indicative of minimum requirements of the materials properties. The use of materials having better properties is not prejudiced by the details above, provided materials for components in bearing contact with each other do not entail galling, corrosion, magnetic induction, etc.

## **2** IS 6603 is under revision and designations referred here are likely to be aligned with IS 1570 (Part 5) in the revision.

**8 SELECTION OF CENTRIFUGAL JET PUMP**

Centrifugal jet pump shall be selected according to IS 12699.

**9 PERFORMANCE CHARACTERISTICS**

**9.1 Factor Affecting Performance**

The submergence of jet pump (assembly) below water level affects the overall performance of the centrifugal jet pump. All the capacities shall be given for the pump offset from well of 1.5 m for horizontal jet and the submergence of jet pump (assembly) shall be specified by the manufacturer along with minimum operating pressure. The method of obtaining higher submergence by supplying the input water to the jet pump (assembly) foot valve through pressure tank shall be as given in Annex Band Fig. 5. Submergence is the level of water above the nozzle of the jet unit.



*Key*

|  |  |  |  |
| --- | --- | --- | --- |
| 1) | Pump | 6) | Gatevalve-3 |
| 2) | Gatevalve -1 | 7) | Collectingtank |
| 3) | Pressuretank | 8) | Pressuregauge*G*1 *-*(ejector head) |
| 4) | Gatevalve-2 | 9) | Pressuregauge*G*2**-**(total head) |
| 5) | Monosetjet centrifugal pump combination | 10) | Pressuregauge*G*3 *-*(submergence) |

NOTE— Netejector head= (G1+ Z) (G3+ Z)

 Nettotal head= (G2+Z)—(G3 + Z )

Fig.5 Installation for Typical Test Setup for Jet Centrifugal Pump Combination with Submergence

**10 TESTING**

**10.1 Method of Testing**

Centrifugal jet pump shall be fitted with the jet assembly through proper sizes of pipes of required lengths with respective orifice plates. One pressure gauge shall be fitted to the delivery pipe of the jet assembly which is the suction pipe of the centrifugal pump. Another pressure gauge shall be fitted to the discharge pipe (delivery pipe of centrifugal pump) of the centrifugal jet pump. By throttling the discharge valve, the following readings shall be taken:

1. Total head (on the pressure gauge connected to the discharge pipe which is delivery pipe of centrifugal pump);
2. Corrected ejector head (on the pressure gauge connected to the suction pipe of the centrifugal pump which is the delivery pipe of the jet pump (Assembly);
3. Discharge;
4. Power input;
5. Speed of the motor;
6. Voltage; and
7. Current.

The above readings shall be tabulated in the form of a test report for each pump as given in Table 2.

At least three test points, that is, duty point, maximum and minimum head shall be taken. The manufacturer shall give the maximum jet setting depth (ejector head + 6m) for the various types of pumps offered at which the maximum ejector efficiency is obtained. All the heads, discharge and power shall be corrected to the rated frequency in case of electric motor driven pumpset and rated speed in case of engine driven pumpset.

**10.2 Testing Method for Centrifugal Jet Pump for Including Pipe Friction by the Use of Orifice Plate**

The depth to low water level, total head, discharge and power input shall be declared by the manufacturer at the duty point and the testing shall be carried out only for the duty point declared by the manufacturer.

Orifice plates as shown in Fig. 6 with diameters calculated in accordance with the procedure given in Annex C shall be used in the pressure pipe and the delivery pipe (suction pipe of centrifugal pump) of the centrifugal jet pump to take into account the field friction. Examples are given in Annex C with Fig. 5, 8, 10, 11, 12 and 13 which give the schematic and test set up diagram for twin, packer and duplex type centrifugal jet pump.

**10.3** Pump casing shall be of robust construction and shall be hydraulically tested to withstand 1.5 times the maximum discharge pressure for 1 min.

1. D



Fig.6 SymmetricalOrificePlate

**13.2 Standard Marking**

The product(s) conforming to the requirements of this standard may be certified as per the conformity assessment schemes under the provisions of the *Bureau of Indian Standards Act*, 2016 and the Rules and Regulations framed there under, and the products may be marked with the Standard Mark.

**Table 1 Performance of Twin Type Centrifugal Jet Pump**

(*Clause* 9.3)

All dimensions in millimetres

(Single phase/Three phase)

|  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- |
| **Rating** | **JetUnitCode** | **PressurePipeDia.** | **DeliveryPipeDia.OfJetAssembly(SuctionPipeofCentrifugalPump)** | **DischargePipeDia(DeliveryPipe of****CentrifugalPump)** | **Minimum clearBoreDia** | **MinimumOperatingPressure/DischargeHead(DeliveryHeadofCentrifugal****Pump)** | **CapacityforDifferentDepthstoLowWaterLevelfromCentrifugalPumpCentre** |
| mm | mm | mm | mm | m | Litres per hour (LPH) |
| 9m | 15m | 25monwards |
| (1) | (2) | (3) | (4) | (5) | (6) | (7) | (8) | (9) | (10) |
|  |  |  |  |  |  |  |  |  |  |

NOTE**—**DepthtoLowWaterLevel(DLWL)mentioned incol(8),(9)and(10)areonlyindicativeandshalldependupontheindividualmodelsandthe respective DLWLranges.

**Table 1APerformance of Packer/Duplex Centrifugal Jet Pump**

(*Clause*9.3)

All dimensions in millimetres

(Singlephase/Three phase)

(Type:Packer/Duplex)

|  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- |
| **Rating** | **JetUnitCode** | **OuterPipeDia** | **InnerPipeDia** | **PressurePipeDia** | **DischargePipeDia(Delivery PipeDiaofCentrifugalPump)** | **MinimumClearBoreDia** | **MinimumOperatingPressure /Discharge Head(DeliveryHeadofCentrifugalPump )** | **CapacityforDifferentDepthstoLowWaterLevelfromCentrifugalPumpCentre** |
| **Litres per hour (LPH)** |
| mm | mm | mm | mm | mm | m | 9 m | 15 m | 25 m onwards |
| (1) | (2) | (3) | (4) | (5) | (6) | (7) | (8) | (9) | (10) | (11) |
|  |  |  |  |  |  |  |  |  |  |  |

NOTE — Depth to Low Water Level (DLWL) mentioned in col (9), (10) and (11) are only indicative and shall depend upon the individual models and the respective DLWL ranges.

**Table 2 Test Report for Contrifugal Jet Pump**

(*Clause* 10.1)

All dimensions in millimetres

|  |  |  |
| --- | --- | --- |
| Single/ThreePhaseRef: | kW/HP: | Pipesizeinmm : |
| Nameofthemanufacturer : | CentrifugaljetpumpSI.No.: | Duplex/PackerType : |
| Dischargein1/h : | Boresizeinmm: | Outer/Inner/Pressuredischarge(Centrifugalpumpdelivery): |
| MaximumjetODinmm: | Totalhead inm: | Twintypejetpump: |
| Depthtolowwaterlevel(DLWL): | Frequency: | Jetdelivery/Pressuredischarge(Centrifugalpumpdelivery): |
| Ratedspeedinrev/min: |  |  |

|  |  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- | --- |
| **Sl. No.** | **Speed** | **Depth to Low Water Level** | **Total Head** | **Actual Discharge** | **Voltage** | **Current** | **Moter****Input** | **Performance at Rated Speed** | **Remarks** |
|  |  | Ejector Head | Correc-tion on head | DLWL | Discharge Gauge Reading | Correc-tionon Head | Total Head |  |  |  |  | Rated DLWL | Rated Total Head | Rated Discharge | Rated Motor Input |  |
| G1 | Z1 | G1+ Z1 | G2 | Z2 | G2+ Z2 |
| rev/min | m | m | m | m | m | m | m | 1/h | V | A | kW | m | m | 1/h | kW |  |
| (1) | (2) | (3) | (4) | (5) | (6) | (7) | (8) | (9) | (10) | (11) | (12) | (13) | (14) | (15) | (16) | (17) |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
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|  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |



Fig.7 Field Installation Diagram for Vertical Twin Type Centrifugal Jet Pump



Fig.8 Testing Installation Diagram for Twin Type Centrifugal Jet Pump



*A* = Horizontal length of pressure pipe, 3 m

*B =* Horizontal length of delivery pipe, 3 m

\*Horizontal length includes equivalent length for bends also.

FIG. 9 FIELD INSTALLATION FOR HORIZONTAL DUPLEX TYPE CENTRIFUGAL JET PUMP



*Key*

|  |  |  |  |
| --- | --- | --- | --- |
| 1) | Priming unit | 7) | Clamp |
| 2) | Pressure control gate valve | 8) | Jet venturi |
| 3) | Orifice plates *d*a and *d*d | 9) | Nozzle |
| 4) | Mono pump | 10) | Foot valve |
| 5) | Slipcoupling | 11) | Strainer |
| 6) | Duplexhead/well adopter |  |  |

Fig.10 Testing Installation for Duplex Type Centrifugal Jet Pump for Factory Setup



*Key*

*G*1Pressuregaugefittedinsuctionpipeofcentrifugalpumpwhichisthedeliverypipeofjetpump.

*G*2Pressuregauge fittedindischargepipe.

NOTE — Ejectorhead=*G*1*+Z ,*Totalhead= *G*2*+Z*

Fig.11 Schematic Testing Arrangement of MonosetCentrifugal Jet Pump



|  |  |  |  |
| --- | --- | --- | --- |
|  | Monopump |  | Pressurecontrol gauge valve |
|  | Jetunit |  | Pressuregauge*G*1and*G*2 |
|  | Footvalve with strainer pipe of jet pump (*D*d) |  | Suctionpipe of centrifugal pump/delivery |
|  | Primingunit |  | Pressurepipe (*D*P*)* |

NOTE—Theorificeplateshallbeinstalledataminimumdistanceof10*D*frombendontheupstreamsideandpressuregaugeshallbeinstalledatminimumof4*D*onthedownstreamsideoforificeplate.

Fig.12 Testing Installation for Horizontal Twin Type Centrifugal Jet Pump



|  |  |  |  |
| --- | --- | --- | --- |
|  | Primingunit |  | Clamp |
|  | Pressurecontrol gate valve |  | Jetpump venturi |
|  | Orificeplates*d*a and*d*d |  | Nozzle |
|  | Monopump |  | Footvalve |
|  | Slipcoupling |  | Deliverypipe of jet pump/suction pipe of centrifugal pump (*Dd*) |
|  | Packer/Duplexhead |  | Equivalentpressure pipe (*D*a) |

Fig. 13 Testing Installation for Packer/Duplex Type Centrifugal Jet Pump

**ANNEXA**

(*Clause*2)

**LIST OF REFERRED INDIAN STANDARDS**

| *IS No.* | *Title* |
| --- | --- |
| IS 210:2009 | Grey iron castings—Specification (*fifth revision*) |
| IS 304:1981 | Specification for high tensile brass ingots and castings (*second revision*) |
| IS 318:1981 | Specification for leaded tin bronze ingots and castings (*second revision*) |
| IS 694:2010 | Polyvinyl chloride insulated unsheathed and sheathed cables/cords with rigid and flexible conductor for rated voltages (*fourth revision*) |
| IS 6595 (Part 1) : 2018 | Horizontal centrifugal pumps for clear, cold water—Specification: Part 1 Agricultural and rural water supply purposes (*fourth revision*) |
| IS 6603:2001 | Stainless steel bars and flats—specification (*first revision*) |
| IS 7347:1974 | Specification for performance of small size spark ignition engines |
| IS 7538:1996  | Three-phase squirrel cage induction motors for centrifugal pumps for agricultural application— Specification (*first revision* |
| IS 9079:2018  | Monoset pumps for clear, cold water for agricultural and water supply purposes— Specification (*third revision*) |
| IS 10001:1981 | Performance requirements for constant speed compression ignition (diesel) engines for general purposes (up to 20 kW) |
| IS 10572:1983  | Methods of sampling for pumps |
| IS 11170:1985 | Specification for 1 performance requirements for constant speed compression ignition (diesel) engines for agricultural purposes (up to 20 kW) |
| IS 12699:1989  | Selection, installation, operation and maintenance of jet centrifugal pump combination— Code of practice |
| IS 14582 : 2021 | Single-phase small ac electric motors for centrifugal pumps for agricultural applications |
| IS 15999 (Part 1) : 2021 | Rotating electrical machines: Part 1 Rating and performance |

**ANNEX B**

(*Clause* 9.1)

**METHOD OF TESTING CENTRIFUGAL JET PUMP WITH REQUIRED SUBMERGENCE**

**B-1 GENERAL**

The submergence of the jet unit below the water level affects the performance of centrifugal jet pump drastically. A jet assembly with inadequate submergence causes cavitation at the mixing point and great loss in performance.Every pump has to be declared with the required submergence for optimum performance of the centrifugal jet pump.In the test set up, it becomes sometimes impractical to locate the jet unit with the required submergence since it is very high.In order to stimulate a pressure tank is used in the test set up as shown in Fig.5:

1. A pressure tank of atleast 5 to 6 times the maximum discharge capacity of centrifugal jet pump in litres/min to be tested;
2. A centrifugal pump with a head of atleast 15 times that of the maximum submergence pressure to be created in the pressure tank, with a discharge capacity of atleast twice the maximum discharge of centrifugal jet pump.

The pressurizing centrifugal pump (1) is connected to the pressure tank through throttle valve (2) and foot-valve. The pressure tank is connected to the centrifugal jet pump through throttle valve (4) at the foot-valve entry. A pressure gauge (10) reads the pressure (G3) at the entry to centrifugal jet pump. A pressure guage (8) reads the ejector head pressure (G1) in the delivery pipe of jet pump (assembly) which in turn is the suction pipe of the centrifugal pump of centrifugal jet pump. A pressure gauge (G2) reads the total head developed by the centrifugal jet pump. Orifice plates are introduced in the pressure and delivery pipes,to take care of field pipe friction (see Fig. 5).

**B-2TESTINGPROCEDURE**

The pressurizing centrifugal pump (1) is started and the valves (2) and (4) are adjusted such that the gauge (10) shows a head nearer to the required declared submergence. The throttle valve (6) is adjusted in such a way that gauge (G1) shows the ejector head nearer to the duty point ejector head plus submergence. Adjust the valves (2) and (4) such that a steady reading of G3 (duty point submergence) and G1 (duty point ejector head + G3) is reached.

Then, measure Q1, the volume rate of flow, with the help of collecting tank and power input to the pump. Then, the head readings for given submergence of G3 are:

(G2+ Z) — (G3+Z) = Total head

(G1+Z)—(G3+Z)= Ejectorhead

**ANNEX C**

(*Clause*10.2)

**TESTINGMETHODFORCENTRIFUGALJETPUMPINCLUDINGPIPEFRICTIONBYTHEUSEOFORIFICEPLATESINTESTSETUP**

* 1. **GENERAL**

Theeffectoffrictioninthelengthofdeliverypipeandpressurepipeinthecentrifugaljetpumpisstimulatedbymeansoforificeplatesinthedeliveryandpressurepipes.Thediameteroftheorificeplateis found bymeansofequatingtheheadlossinfrictioninthecorrespondingpipelengthsinfieldusetotheheadlossbysuddencontractionandexpansionbytheintroductionoforificeplates.

Fortwintypepumps,theorificeplatesareintroducedinthecorresponding pipelengthsinthetestsetup.Forpackertypepump,thelossinfrictionisfoundfortheannularareabetweentheouterpipeandthedeliverypipeintermsof anequivalentdiameterofapressurepipe,andinthispipe,theorificeplateisintroduced.ThemethodoflocatingorificeplatesinthetestsetupisshowninFig.5,8,10,11,12and 13fordifferenttypesofpumps.Themethodsforcalculatingthediameteroforificeplateshallbeasgivenin**C-2**to**C-4**.Thenominalpipesizeandcorrespondingpipeinner diameterforcalculationoforificeplatesaregiveninTable3.

* 1. **SELECTION OF ORIFICE DIAMETER**

**C-2.1 Terminology**

*L* = length of pipeline;

*D*d = inner diameter of delivery pipe of jet unit for twin, packer and duplex;

*D'*d = outer diameter of delivery pipe of jet unit for duplex and packer only; and

*D*p = inner diameter of pressure pipe;

*Do*=inner diameter of outer pipe in duplex/packer type pump;

*dp, dd, da* =inner diameter of orifice plates for pressure pipe, delivery pipe and equivalent pipe, respectively;

*h*f *=* head loss in friction in the length;

*h* = head loss in orifice plate;

*f* = Darcy­weisbach friction factor,

*C* = discharge coefficient;

*α* = *CE=*flow coefficient;

*β* = (*dd*/*D*d) or (*d*P/*D*P) or (*d*a/*Do*) = diameter ratio of orifice plate to pipe inner diameter;

*E* = Velocity approach factor$= \left(1-β^{4}\right)^{-1/2}$

ρ = Mass density = *w/g;*

*Q* = *qm/p* = volume rate flow; and

$V = \frac{Q}{\left(\frac{π}{4}\right)D^{2 }}$= *Q/A*

where

*A* = area of pipe

Δ*p*= pressure loss in orifice plate

Δ*p/w* = head loss in orifice plate

**Table 3 PipeInnerDiameterforNominalSizesofPipes**

(*Clause*C-1)

All dimensions in millimeters

|  |  |  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- | --- | --- |
| **NominalPipe Sizesin mm** | 20 | 25 | 32 | 40 | 50 | 65 | 80 | 100 |
| **Pipeinnerdiameter for calculationof orificeplatesinmm** | 22 | 27 | 36 | 42 | 53 | 69 | 81 | 106 |

**C­2.2**Theaveragevalue of*C*=0.6and*f* =0.0278hasbeentakenafterconsideringthedifferentdiametersofpipediameter ratio andlifeofpipe. A10percenterrorintheaboveresultsaffectsonlytheoverallresultofpumpperformancebyonepercent.

If*d*istheorificeplateinnerdiameter:

*qm*=α$\left(\frac{π}{4}\right)$*d*2√2(Δpp)

Substituting

*qm*= *PQ*

*Q= CE*$\left(\frac{π}{4}\right)$*d2*$\sqrt{2(∆ p^{ρ/ρ^{2}})}$

= *CE*$\left(\frac{π}{4}\right)$*d2*$\sqrt{2(∆ p/w)g}$

= *CE*$\left(\frac{π}{4}\right)$*d2*$\sqrt{2gh}$

= *CE*$\left(\frac{π}{4}\right)$*D2*𝛽2$\sqrt{2gh}$

= *CE*𝛽2$\left(\frac{π}{4}\right)$*D2*$\sqrt{2gh}$

*Q*= *CE*𝛽2*A* $\sqrt{2gh}$

But *Q/A = V*, therefore squaring both the sides andequating, we get:

$$ h = \left(\frac{V^{2}}{2g}\right)×\left[\frac{1}{C^{2}\left(Eβ^{2}\right)^{2}}\right]$$

But

$$Eβ^{2 } = \frac{β^{2}}{\left(1-β^{4}\right)^{1/2}}$$

$$ = \frac{1}{\left(\frac{1}{β^{4}}-1\right)^{1/2}}$$

$$\left(Eβ^{2}\right)^{2} = \frac{1}{\left(\frac{1}{β^{4}}-1\right)}$$

$$ h =\left[\left(V^{2 }/2g\right)\right]\left[\frac{\left(\frac{1}{β^{4}}-1\right)}{C^{2}}\right]$$

For any pipe,Allowingforpressurerecoveryafterorificeplates,wecanwrite:

K\**h*=*h*fWhere*K*is 0.9 up to 40 mm sizes of pipe and 0.8forhigherpipesizes.

$$h\_{f}= \left[\left(fL/D\right)×\left(\frac{V^{2}}{2g}\right)\right]$$

We get

$$\frac{1}{β^{4}}= \left[C^{2}f \left(L/KD\right)+1\right] from \left[C^{2}f\left(L/KD\right)\right]$$

$$ = \left(\frac{1}{β^{4}}-1\right)$$

Substituting

*β*$ =$ *d/D*

$$\frac{D^{4}}{d^{4}} = \left[C^{2 }f\left(L/KD\right)+1\right]$$

$$d = \frac{D}{\left[C^{2}f\left(L/KD\right)+1\right]^{0.25}}$$

Substitutingvalueof*C=*0.6and*f*=0.0278,thefinalequationforthediameteroforificeplateas:

$$ h= \frac{D}{\left[\left(10L/KD\right)+1\right]^{0.25}}$$

Thismeansthatif*D*is diameter in millimeters ofthepipeusedinthefieldforthesystemand*L*isitslengthinmeters,theequivalentfrictionlossshallbecreatedbyusinganorificeplateofdiameter*d.*Itshallbenotedthatwhileusingthisequation,*L*valueshallbetakenasthelengthofpipeinthefieldminusthelengthofpipeusedin factorysetupforsubstitutingintheequation,equivalentfrictionlossshallbecreatedbyusinganorificeplateofdiameter*d.*

* 1. **DIAMETEROFORIFICEPLATEFORTHEANNULARAREAOFPACKER/DUPLEXTYPEPUMP**

Thefrictionallossintheannularareaforthepressure pipeportionofapacker/duplextypepumpis given by:

$$h\_{f}= f\left[\frac{L}{\left(D\_{o}-D^{'}\_{d}\right)}\right]\left[\frac{Q}{\frac{π}{4}\left(D\_{o}^{2}-D^{'}\_{d}^{2}\right) × \left(\frac{1}{2g}\right)}\right]$$

$= \left[\frac{Q^{2}}{\left(\left(\frac{π}{4}\right)^{2 }× 2g\right)}\right]× \left[\frac{L}{\left(D\_{o}-D'\_{d}\right)\left(D\_{o}^{2}-D'\_{d}^{2}\right)}\right]$ (1)

Ifanequivalentpipeofinnerdiameter*D*aandlength*L*eisselectedtogivethesameamountofheadlossinfrictionasa single pipe:

$$h\_{f} = fL\_{e}\left(\frac{1}{D\_{a}}\right) × \left[\frac{Q^{2}}{\left(\frac{π}{4}\right)^{2}× D\_{a}^{4}}\right]× \left(\frac{1}{2g}\right)$$

 $\_{}$

$$ h\_{f} =\left[\frac{fQ^{2}}{\left(\frac{π}{4}\right)^{2}× 2g}\right]× \left(\frac{L\_{e}}{D\_{a}^{5}}\right)……. (2)$$

Equatingequations(1)and(2),weget

$$\left(\frac{L\_{e}}{D\_{a}^{5}}\right)= L × \left[\frac{1}{\left(D\_{o}-D'\_{d}\right)\left(D\_{o}^{2}-D'\_{d}^{2}\right)^{2}}\right]$$

*D'*disouterdiameterofthedeliverypipeofjetunitforpacker/duplex

$$L\_{e}=D\_{a}^{5} × \left[\frac{L}{\left(D\_{o}-D^{'}\_{d}\right)\left(D\_{o}^{2}-D^{'}\_{d}^{2}\right)^{2}}\right]$$

Sointhepacker/duplextype,theorificeplateissetinahorizontallengthabovetheduplex/packerheadusingapipeofconvenientdiameter*D*aforthepressurepipe.Forthispipe diameter,theequivalentlength*L*eiscalculatedfortheannularactualpipelength, *L*,usedinthefield.

Thentocreatethefrictionalloss,anorificeplateofdiameter*d*a,isselectedsothat:

$$d\_{a} = \left[\frac{D\_{a}}{\left[C^{2}\left(\frac{fL\_{e}}{D\_{a}}\right)+1\right]^{\frac{1}{4}}}\right]$$

Where*L*is in metersand*D*isinmillimeters.Then:

$$d\_{a}= \left[\frac{D\_{a}}{\left[\left(\frac{10L\_{e}}{KD\_{a}}\right)+1\right]^{\frac{1}{4}}}\right]$$

Diameteroforificeplatetobeusedinthehorizontalequivalentpressurepipelineis:

$$d\_{a} = \left[\frac{D\_{a}}{\left[\left(\frac{10L\_{e}}{KD\_{a}}\right)+1\right]^{\frac{1}{4}}}\right]$$

**C-4 MODEL CALCULATIONS FOR SELECTION OF ORIFICE PLATE OF TWIN TYPE JET PUMP**

**C– 4.1Example1**

*See*Fig.6and7. Calculatethe diameteroforifice platestobeusedintwintypecentrifugaljetpumpofsize50mm×40mm-deliverypipeofjetassembly(suctionpipeofcentrifugalpump)×pressurepipes.

Thedutypointgroundtolowwaterlevel is25mandatdutypoint,thepumprequiresfourmetressubmergenceandthepumpisaverticalpumphavingonemetrepipeabovethegroundlevel,mediumclasspipesareusedinthefactorysetup,threemetrelengthisusedfortestingwith 2.5msubmergence.

 *Lf*= Length ofpipeusedinfield

=Ground tolowwaterlevel+submergence+verticaldistanceabovethegroundleveltocentrifugalpump

=25+4+1 =30m

 *L*=Lengthofpipetobetakenforfrictioncalculation

=Pipe length used infield$– $pipelengthusedintestsetup

=30$ -$ 3=27m

Theinnerdiameterof50mmmedium classpipeis:

*D*d= 53mm

Theinnerdiameter of40mmmediumpipeis:

*D*p= 42mm

Thediameteroforificeplateforthedeliverysideofthejetpump(whichinturnisthesuctionpipeofcentrifugalpump)

*d*d= Diameteroforificeplateinjetpump(assembly)delivery,whichisthesuction pipeofcentrifugalpump.

*d*d$=\frac{D\_{d}}{\left[\left(\frac{10L}{KD\_{p}}\right)+1\right]^{\frac{1}{4}}}$

$$=\frac{53}{\left[\frac{270}{\left(0.9×53\right)+1}\right]^{\frac{1}{4}}}$$

$ = $32.99 mm

Sincethelengthofthepressurepipealsoisthesame,diameteroforificeplateinpressurepipe:

$$d\_{p}=\frac{D\_{p}}{\left[\left(\frac{10L}{KD\_{p}} + 1\right)\right]^{\frac{1}{4}}}$$

$$=\frac{42}{\left[\left(\frac{270}{0.9}\right) × 42 + 1\right]^{\frac{1}{4}}}$$

=24.86mm

Sotheabovesizeoforificeplatesarefittedtothedeliverypipeofjetpump(assembly)whichisthesuctionpipeofcentrifugalpumpandpressurepipeofjetpump(assembly).Itisalwaysconvenienttohavethecentrifugalpumpsinahorizontalpositionforbothverticalandhorizontalsetsforeasytest setup.

**C– 4.2Example2**(*see*Fig.3and8)

Calculatethediameteroforificeplatesforthesame centrifugaljetpumpifitisofahorizontalpackertype/duplextypeusingan80mmouterpipe,50mm inner pipe and in the horizontal position it uses50 mm equivalent pressure pipe.Thelengthofverticalconcentricpipeusedinthefieldis25mgroundtolowwaterlevel, fourmetressubmergenceandthreemetreshorizontalpipesof50mmeach,includingtheequivalentlengthforthebend.Inthefactorytestsetup,thelengthofconcentricpipesusedisthreemetresandinthehorizontalportiontwopipesof50mmoftwometreslengthisusedincludingtheequivalentlengthforbends.Inallcases,mediumclasspipesareused.Thesubmergenceatfactorysetupis2.5m.Thepumpcentrelineinbothfieldandfactorysetupabovegroundlevelisonemetre.

Calculation:For the innerpipe;

Lengthofinnerpipeatfield=25+4+ 4 =33m

Lengthofpipeusedinfactorysetup =2+1+3 =6m

Lengthofpipe*L*dusedforfrictioncalculation

33–(2+1+3)=27m

(ReferFig.9andFig.10)

*Dd*=Inner diameterofinnerpipe=53mm

That is,deliverypipeofjetpump.Therefore,diameteroforificeplate:

$$d\_{p} =\frac{D\_{p}}{\left[\left(\frac{10L\_{d}}{KD\_{p}} + 1\right)\right]^{\frac{1}{4}}}$$

For the annular pipe:

*Do*=Inner diameterofouterpipeof80mm

 =80.8mm

*D*d*=*Outerdiameterofinnerpipewhichisthe deliverypipeofjetpump

 =60.3mm

Lengthofconcentricpipe usedinthefield25+4 =29m

Lengthofpipeusedinthefactorysetup =3 m

$Le$ = Lengthtobetakenforcalculatingfriction= 29$– $3=26m

Let, *D*e= Diameterofequivalentpipe

=Diameterof pipe usedinpressure pipe

 =53mm

## This equivalentlengthforpressurepipe:

##  $Le= \left(D\_{a}\right)^{5}× \frac{L}{\left[\left(D\_{o}-D'\_{d}\right)\left(D\_{o}^{2}-D'\_{d}^{2}\right)^{2}\right]}$

$$=\left(53\right)^{5}× \frac{26}{\left[\left(80.8-60.3\right)\left(80.8^{2}-60.3^{2}\right)^{2}\right]}$$

$=63.39 $m

Length*L*etobetakenforfrictioncalculation:

= *L*'e+(3+1 – 2 – 1)

=64.39m

Diameteroforificeplatetobeusedinequivalentpipefortheannulararea:

 $$ = \frac{53}{\left(\frac{643.9}{0.8×53}+1\right)^{\frac{1}{4}}}$$

$= 26.42 $mm

**ANNEX D**

(*Clause* 11)

**EXAMPLE TO CHECK THE DECLARED VALUES**

**D–1**A centrifugal jet pump of nominal 0.75 kW rating has following declared values:

DLWL : 25m

DLWLrange : 18mto30m

Discharge : 10001/h

Totalhead : 44m

Power input : 1.2kW

Maximumcurrent: 6.0A

Inthisfigurelineshavebeendrawngivenforthedeclaredvaluesandalso92percentofdischarge,92percentoftotalhead,92percentofDLWL,110percentofpowerinputandfor107percentofthemaximumcurrentdeclaredintheDLWLrange.Characteristiccurveshavebeendrawnoffourjetpumpsofabovedeclaredvalues.Thehatchedportionsshowninthefigureshowtheareasofdeviationpermitted(onthenegativeside)inrespectofdischarge*vs*DLWLanddischargevstotalhead.

If the characteristic curve passes through the hatchedportion or is above the hatched portion the samplepump conforms to the requirements. Similarly if thedischarge vs input, power curve is below 110 percentline, that is, in this case 1.32 kW (= 1.2kW × 1.1)at the duty point of 1 000 1/h the sample pump satisfiesthe requirements. Thus of the four pumps whosecharacteristic curves are given in the Fig. 14, Fig. 15 and Fig. 16.

1. Sample1: Satisfiestherequirements
2. Sample2: Fails ininputpower,sinceat thedutypointtheinputpoweris1.34kW
3. Sample3: FailsindischargevsDLWL

iv) Sample4:Failsinmaximum currentintheoperating rangeofDLWL



Fig. 14 Input Power Vs Discharge



Fig. 15 Discharge Vs DLWLand Total Head



Fig. 16 Discharge Vs Current andDepth to Low Water Level

**Annex E**

(*Foreword*)

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*Member Secretary*

Shri AmanDhanawat

Scientist ‘B/Assistant Director

 (Mechanical Engineering), BIS

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